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# High-throughput Identification of Highly Active and Selective Single-Atom Catalysts for Electrochemical Ammonia Synthesis through Nitrate Reduction

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## Abstract

The highly selective and active nitrate-to-ammonia electrochemical conversion ( $\text{NO}_3$  reduction reaction [ $\text{NO}_3\text{RR}$ ]) can be an appealing and supplementary alternative to the Haber-Bosch process. It also opens up a new idea for addressing nitrate pollution. Previous study

demonstrated that FeN<sub>4</sub> single-atom catalyst (SAC) indicates excellent NO<sub>3</sub>RR performance. Nonetheless, the mechanism that triggers the electrocatalytic NO<sub>3</sub>RR remains unclear. The feasibility of NO<sub>3</sub>RR over various SACs is verified in this study via high-throughput density functional theory calculations with the single transition metal (TM) atom coordinated with four nitrogen atoms supported on graphene as the example. We conducted a comprehensive screening of TM SAC candidates for stability, NO<sub>3</sub><sup>-</sup> adsorption strength, catalytic activity, and selectivity. Results reveal that the most promising candidate among the 23 TM SACs is Os SAC with a low limiting potential of -0.42 V. Os SAC is better than Fe SAC with a limiting potential of -0.53 V because of the strong interaction between the oxygen of NO<sub>3</sub><sup>-</sup> species and Os atom. The origin of high NO<sub>3</sub>RR activity of Os SAC is explained by its inner electronic structure of the strong hybridization of the Os atom and NO<sub>3</sub><sup>-</sup> caused by the increasing charge transfer from TM atom to NO<sub>3</sub><sup>-</sup>, leading to the suitable NO<sub>3</sub><sup>-</sup> adsorption. This research provides a fundamental insight of discovering novel NO<sub>3</sub>RR catalysts and may provide a motivating drive for the creation of effective ammonia electrocatalysts for further experimental investigation.

**Key words:** high-throughput calculations, single-atom catalysts, nitrate reduction, ammonia synthesis, electrocatalysis

## Introduction

The discharge of domestic sewage has increased sharply with the development of industries and agriculture and the continuous growth of the population. The concentration of nitrate (NO<sub>3</sub><sup>-</sup>) in drinking water has been rising, causing major pollution of water resources, serious harm to human health, and terrible diseases, such as cancer and blue baby syndrome.<sup>1,</sup>

<sup>2</sup> The removal of nitrate pollution in broad groundwater areas is a global issue because of the excellent stability of nitrate under normal aerobic conditions. According to the principle of remediation, the current treatment methods for a small part of groundwater nitrate pollution are divided into three categories: physical and chemical remediation technology, bioremediation technology, and chemical reduction technology. However, cleaning huge areas of nitrate pollution from groundwater, which is still a longstanding and tedious task, is a global issue.<sup>3</sup> Finding an effective and environmentally friendly way to treat nitrate wastewater is critically required; thus, it has become a popular research issue.

Alternatively, electrochemical  $\text{NO}_3^-$  reduction reaction ( $\text{NO}_3\text{RR}$ ) for ammonia ( $\text{NH}_3$ ) synthesis is regarded as a potential strategy for converting  $\text{NO}_3^-$  based on electrochemical technologies to eliminate nitrate contaminants in wastewater.<sup>4-7 8,9</sup> In addition,  $\text{NH}_3$  is one of the most fundamental chemical raw materials and an essential energy storage medium.<sup>10-14</sup> However, traditional industrial-scale synthesis of  $\text{NH}_3$  still has many drawbacks, such as harsh reaction conditions requiring high temperature (400–500 °C) and high pressure (150–300 atm), and the use of traditional energy sources, such as coal, generates a large amount of  $\text{CO}_2$  emissions; this scenario is not conducive to the sustainable development of energy and the environment.<sup>15-18</sup> Furthermore, the industrial targeted product of electrochemical methods to remove nitrate contaminants is mainly  $\text{N}_2$ , with  $\text{NH}_3$  as the by-product.<sup>19-22</sup> In particular,  $\text{NO}_3\text{RR}$  provides a competitive route for ammonia ( $\text{NH}_3$ ) synthesis by transferring nine protons and eight electrons ( $\text{NO}_3^- + 9\text{H}^+ + 8\text{e}^- \rightarrow \text{NH}_3 + 3\text{H}_2\text{O}$ ), which is essential for low-temperature ammonia synthesis.<sup>23,24</sup> Thus, developing high-performance electrocatalysts to convert nitrate waste into value-added  $\text{NH}_3$  selectively is a promising strategy for resolving energy and environmental issues. It will also pave the way for a new nitrate treatment method.

Compared with bulk or nanosized transition metal (TM) catalysts, single-atom catalysts (SACs) have sparked considerable research interest in the field of catalysis due to their highest atom usage efficiency and unique atomic structure and electronic characteristics.<sup>25-27</sup> In many catalytic reactions, SACs show outstanding advantages, such as excellent activity, exceptional selectivity, and high stability.<sup>28-36</sup> Recent studies also demonstrated that SACs exhibit excellent performance by anchoring on various substrates,<sup>37-39</sup> which can effectively avoid the problem of metal agglomeration. Among these, covalent organic frameworks (COFs) have been widely used in the design of various SAC electrocatalysts in recent years due to their tunable nanopore size, high accessible surface area, and predesigned building units, abundant active sites, designable chain structures, and programmable topologies.<sup>40,41</sup> Very recently, Zhang, Wang, and Liu, et al. reported that iron-phthalocyanine based COF (denoted as FePc-BBL COF) exhibits unusual oxygen reduction reaction (ORR) activities and fast kinetics with a remarkable half-wave potential of 0.933 V and an ultralow Tafel slope of 24.8 mV dec<sup>-1</sup> in alkaline media. In addition, the FePc-BBL COF also exhibits outstanding zinc-air battery performance when employed as a cathode electrocatalyst.<sup>42</sup> Another work discovered that Co-N-C SAC of metalloporphyrin-based COF exhibits the highest catalytic activity for hydrogen peroxide synthesis with high faraday efficiency at 84%, a large turnover frequency of 9.05 s<sup>-1</sup> per Co site, and productivity of 909 mmol g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>.<sup>43</sup>

NO<sub>3</sub>RR on single-atom catalysts has increasingly been observed in recent years, and various investigations have been reported. The single-atom Cu catalyst was the first proposed TM SAC to reduce nitrate to ammonia considerably via experiment; the strong binding between Cu and N (particularly Cu-N<sub>2</sub>) is the key to favorable adsorption of NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup>.<sup>44</sup> Niu et al. systematically explored the selectivity and activity of a single TM

supported on carbon nitride in the reduction of nitrate to ammonia by performing first-principle calculations; they finally screened out Ti/g-CN and Zr/g-CN because of their strong adsorption of  $\text{NO}_3^-$ .<sup>23</sup> Lv et al. discussed the activity and selectivity of TM/g- $\text{C}_3\text{N}_4$  single-atom catalysts to the electrocatalytic reduction of nitrates to  $\text{NH}_3$  by performing first-principle calculations.<sup>45</sup> Notably, there are still many other excellent works that reported different supporting materials for  $\text{NO}_3\text{RR}$ . For example, Zhao's group demonstrated that Os anchored on graphdiyne was identified as an ideal  $\text{NO}_3\text{RR}$  catalyst with a low limiting potential (-0.37 V) and great suppressing effect on the competing reactions by systematically evaluating the activity and selectivity of various candidates.<sup>46</sup> However, the development of graphitic alkyne in electrocatalysis is limited by its poor electrical conductivity and complex synthesis process. Last year, Li, Zhao and Yu et al. reported that In deposited on Pd nanoparticles shows room-temperature nitrate catalytic reduction activity and proves mechanistic of catalyst performance, but the  $\text{NH}_3$  yield rate and Fradaic efficiency are still unsatisfactory.<sup>47</sup> Graphene, a single-layer two-dimensional carbon material with unique structural and electrical characteristics, has been found to offer excellent support for SACs. Recently, nitrogen-doped graphene supported Fe SAC has been experimentally reported recently as an active and selective electrical catalyst that can convert nitrates to valuable ammonia because of the lack of neighboring metal sites, which can effectively prevent the N-N coupling step required for  $\text{N}_2$  and then promote ammonia product selectivity.<sup>48</sup> Despite the excellent activity and selectivity of SAC for the nitrate reduction to ammonia, research on this topic is still in its early stages. What are the primary variables that influence catalytic selectivity? Why do the activities of various SACs differ considerably? Experiments demonstrated that Fe SAC has excellent activity and selectivity. Hence, does another metal with performance superior to Fe performance exist? Appropriately analyzing the feasibility of

SACs on NO<sub>3</sub>RR and revealing the specific mechanism of SACs are essential to answer the issues mentioned.

The NO<sub>3</sub>RR performance of SACs is extensively examined first in this work by high-throughput first-principle computation using a single TM (from Ti to Au) supported on N-doped graphene-based catalysts (denoted as TM SAC), as shown in **Figure 1b**. A four-step screening method is considered, and the reaction mechanisms that convert NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub> are classified as O-end, O-side, N-end, N-side, and NO-dimer. A volcano map and NH<sub>3</sub> desorption energy are constructed to describe activity patterns on TM<sub>SA</sub> SAC. Among the 23 proposed catalysts, Os SAC is a rather promising catalyst for the electrochemical NO<sub>3</sub>RR to produce NH<sub>3</sub> with efficient activity and selectivity. The limiting potential of Os SAC for NO<sub>3</sub>RR to NH<sub>3</sub> is 0.42 V, which is lower than the limiting potential of experimentally synthesized Fe SAC (0.52 V). Furthermore, the genesis of NO<sub>3</sub>RR activity and the experimental feasibility of Fe SAC and Os SAC are investigated. Our work screens and designs more efficient NO<sub>3</sub>RR catalyst based on the very mature Fe SAC catalyst and also decreases the time and economic cost of trial and error in the NO<sub>3</sub>RR experimental study.

## Results and discussion

### Structure and stability of TM SAC

In recent years, SACs have attracted increasing interest and applications in the field of catalysis owing to their high activity and selectivity. The systems we choose to investigate are SACs supported by nitrogen-doped graphene, which have been extensively studied, realized through experiments, and applied to many catalysis fields.<sup>49</sup> Inspired by the recently synthesized Fe SAC catalyst to reduce NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub>, we studied the catalytic performance of a series of TM SACs. As shown in **Figure 1a**, we employed a four-step screening method to confirm whether TM SAC is suitable for the reduction of nitrate to ammonia and marked the

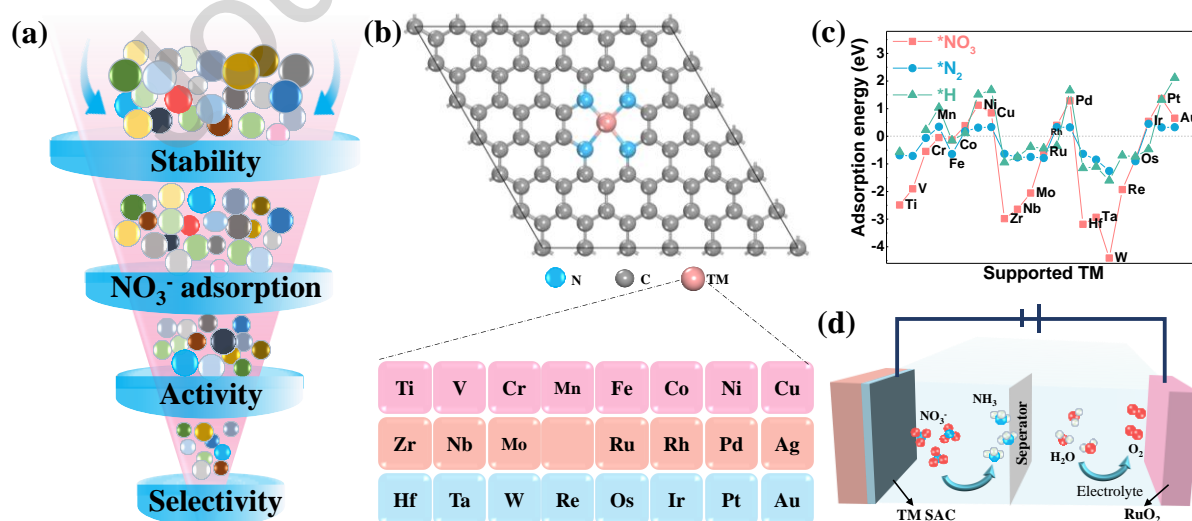
criteria for each step of screening process in detail as shown in **Figure S1**. First, verifying that TM can be stably anchored into the carbon layer is necessary.<sup>50</sup> Second,  $\text{NO}_3^-$  can be stably adsorbed on the TM SAC, which is also a necessary criterion for the entire screening step and can ensure the subsequent reaction.<sup>51</sup> In particular, the adsorption energy of  $\text{NO}_3^-$  must be satisfied:  $\Delta G_{*\text{NO}_3} < 0$ . Third, the catalyst activity screening, that is, the TM SAC with a large limiting potential ( $U_L$ , by calculating the Gibbs free energy), is eliminated. Finally, the selectivity of the remaining catalysts must be confirmed, which is achieved by calculating  $U_L$ , to ensure that the synthesis of  $\text{NH}_3$  in the  $\text{NO}_3\text{RR}$  process has a lower  $U_L$  than that in other competitive reaction products ( $\text{H}_2$ ,  $\text{N}_2$ ,  $\text{NO}$ , and  $\text{NO}_2$ ).<sup>45,48</sup> Subsequently, **Figure 1b** displays that the TM atom coordinated with four nitrogen atoms is joined in graphene to replace two C vacancies. A total of 23 composed systems of TMs are calculated in this work, and the optimized structures are displayed in **Figure S2** (Supporting Information). The geometric structure of TM SACs is retained well. However, some TMs with large radius are out of the plane after full structural relaxation. Furthermore, the thermodynamic stabilities of TM SAC candidates are examined by the binding energy  $E_b$ , which is defined as follows:  $E_b = E_{\text{TM SAC}} - E_{\text{NAC}} - E_{\text{TM}}$ , where  $E_{\text{TM SAC}}$  and  $E_{\text{NAC}}$  represent the total energies of the TM SAC candidate and the pristine substrate, and  $E_{\text{TM}}$  is the energy of the isolated TM atom. As shown in **Figure S3**, our calculated values of  $E_b$  are all well below zero except for Ag SAC. This observation implies the high thermodynamic stability of most TM SAC candidates. Thus, the Ag atom is first ruled out.

### **$\text{NO}_3$ Adsorption on TM SAC**

The initial step in the  $\text{NO}_3\text{RR}$  process is the adsorption of  $\text{NO}_3^-$ , which plays a key role in the whole catalytic reaction. Thus, the adsorption strength of  $\text{NO}_3^-$  on TM SAC must be determined. **Figure S4** depicts the consideration of two possible initial configurations of



$\text{NO}_3^-$  adsorbed on TM centers (1-O and 2-O patterns). As shown in **Table S1**,  $\text{NO}_3^-$  prefers to adsorb on TM SAC via the 2-O pattern (two oxygen atoms adsorbed on TM SAC); the adsorption energy of the 2-O pattern is more negative than that of the 1-O pattern. Furthermore, the adsorption strength of  $\text{NO}_3^-$  on bare graphene is examined. From another perspective, the relatively weak  $\text{NO}_3^-$  adsorption (+1.56 eV) on bare graphene demonstrates the importance of TM active sites in  $\text{NO}_3\text{RR}$  activation. **Figure 1c** depicts the adsorption energies of  $\text{NO}_3^-$  ( $G_{*\text{NO}_3}$ ), H proton ( $G_{*\text{H}}$ ), and  $\text{N}_2$  molecule ( $G_{*\text{N}_2}$ ) on TM SAC. **Figure S5** depicts the corresponding configurations of  $*\text{H}$  and  $*\text{N}_2$ . The negative adsorption energy indicates that the  $\text{NO}_3^-$  adsorption to the TM SAC substrate is a spontaneous exothermic process, which is favorable to the subsequent reaction. On the contrary, if the adsorption energy is positive, then  $\text{NO}_3^-$  cannot be adsorbed on the substrate spontaneously, and follow-up reactions cannot be performed. Except for the TM SAC, including Co, Ni, Cu in 3d, Rh and Pd in 4d, and Ir, Pt, and Au in 5d, the majority of the TM SAC adsorptions of  $\text{NO}_3^-$  are an exothermic process, which proves to be an excellent potential catalyst. The  $\Delta G_{*\text{NO}_3}^*$  values of most candidates are more negative than  $G_{*\text{H}}$  and  $G_{*\text{N}_2}$  values on the TM SAC for the early TM SACs, suggesting that  $\text{NO}_3\text{RR}$  is favorable.

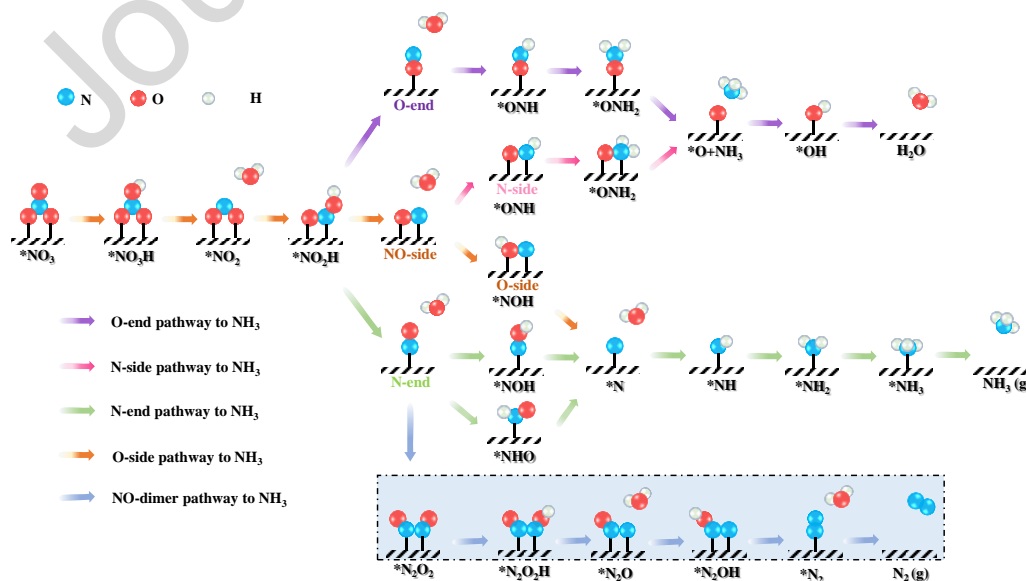


**Figure 1.** a) Schematic illustration of metals considered in this work for screening. b) Top view of the TM SAC atomic structure. Atom labels: C (grey), N (blue), and TM (pink). A list of the screened TM atoms (from Ti to Au) exists. c) Adsorption energies of  $\text{NO}_3^-$ ,  $\text{N}_2$  molecule, and H proton on TM SAC are compared. d) Schematic representation of the proposed electrochemical cell for  $\text{NO}_3\text{RR}$  (cathode: TM SAC) and Oxygen evolution reaction (OER) (anode:  $\text{RuO}_2$ , for example).

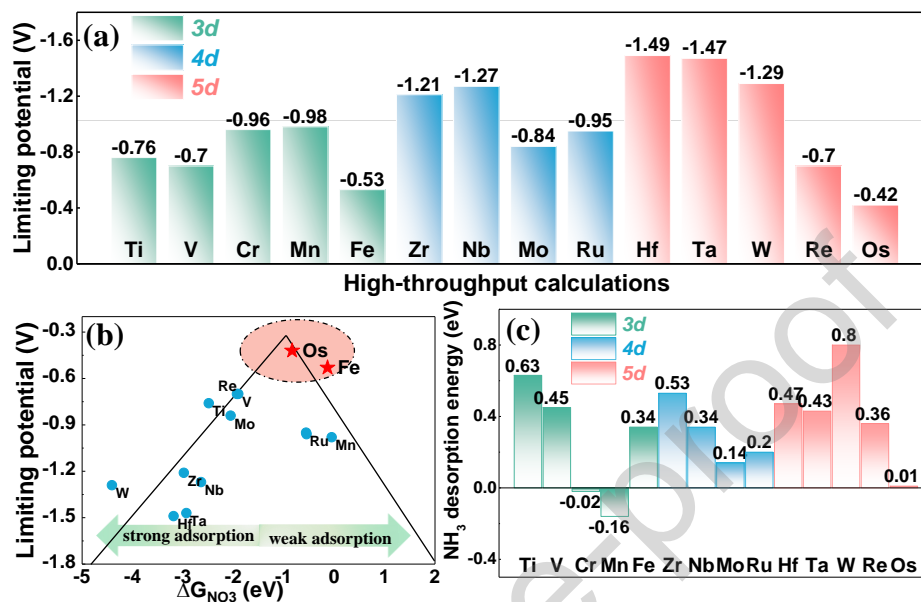
### **$\text{NO}_3\text{RR}$ Mechanism on TM SAC**

The electrochemical conversion of  $\text{NO}_3^-$  to  $\text{NH}_3$  is a complicated process that involves several reaction steps and by-products (for example,  $\text{NO}_2$ ,  $\text{NO}$ ,  $\text{N}_2\text{O}$ , and  $\text{N}_2$ ).<sup>52</sup> **Figure 1d** depicts an electrochemical cell including  $\text{NO}_3\text{RR}$  at the TM SAC cathode and the OER at the anode. Then, we explored the pathway from  $\text{NO}_3^-$  to  $\text{NH}_3$  to understand the entire  $\text{NO}_3\text{RR}$  process.  $\text{NO}$  is adsorbed on the catalytic active site through various adsorption structures based on the pathways provided in the previous study.<sup>23,53</sup> Thus, the ammonia synthesis routes of  $\text{NO}_3\text{RR}$  are classified as O-end, O-side, N-end, and N-side (**Figure 2**). The pathway for producing the by-product  $\text{N}_2$  from  $\text{NO}$  dimers is also considered, as seen in the lower shaded portion of **Figure 2**. We chose the route with the strongest adsorption of various  $\text{NO}$  adsorption modes for the subsequent calculation and analysis of the reaction pathways. Thus, we examined the  $\text{NO}_3\text{RR}$  performance of TM SAC systematically via high-throughput calculations, and the performance criterion is the limiting potential ( $U_L = -G_{max}/e$ , where  $G_{max}$  is the highest value of free energy change in all fundamental steps). **Figure 3a** shows that the  $U_L$  value in the center of each period is lower than that in the left and rightmost ones, demonstrating that they are potential  $\text{NO}_3\text{RR}$  electrocatalysts to produce  $\text{NH}_3$ . The volcano diagram between the limiting potential  $U_L$  and  $\Delta G^*_{\text{NO}_3}$  of different TM SAC catalysts is shown in **Figure 3b**, where Os SAC and Fe SAC are almost located at the top of

the volcano.  $\Delta G^*_{\text{NO}_3}$  is chosen as the descriptor, thus, neither too strong nor too weak  $\text{NO}_3^-$  adsorption energy is beneficial to the completion of the entire reaction; in particular, too weak  $\text{NO}_3^-$  adsorption inhibits the creation of NOH or NHO ( $*\text{NO} + \text{H}^+ + \text{e}^- \rightarrow *\text{NOH}/*\text{NHO}$ ), whereas too strong adsorption leads to difficult reaction pathway for the formation of  $\text{NH}_3$  ( $*\text{NH}_2 + \text{H} + \text{e}^- \rightarrow *\text{NH}_3$ ), which is consistent with earlier studies.<sup>45,23</sup> In addition, the final desorption of ammonia is also an important indicator for evaluating reaction activity.<sup>35</sup> Then, we summarized the Gibbs free energy of  $\text{NH}_3$  desorption ( $\Delta G^*_{\text{NH}_3\text{-des}}$ ) on various TM SAC catalysts, as shown in **Figure 3c**. The  $\Delta G^*_{\text{NH}_3\text{-des}}$  values are all positive except for Cr SAC and Mn SAC, and the promising Os SAC and Fe SAC exhibit the  $\Delta G^*_{\text{NH}_3\text{-des}}$  of 0.34 and 0.01 eV, respectively, indicating that they can release from the active sites spontaneously. This scenario is easier than the previously reported  $\text{NH}_3$  desorption in the literature (0.96 and 1.08 eV for Ti/g-CN and Zr/g-CN; 0.77 eV for Ru/g-C<sub>3</sub>N<sub>4</sub>), which promotes the release of active sites, thereby improving catalytic activity. The above results demonstrate that both Os SAC and Fe SAC are desirable electrocatalysts for  $\text{NO}_3\text{RR}$  to produce  $\text{NH}_3$ ; this finding is consistent with the experimental report indicating that Fe SAC exhibits excellent  $\text{NO}_3\text{RR}$  activity.<sup>48</sup>



**Figure 2.** Detailed pathways of NO<sub>3</sub>RR, including O-end, O-side, N-end, and N-side pathways to NH<sub>3</sub>, as well as NO-dimer pathway to N<sub>2</sub>.

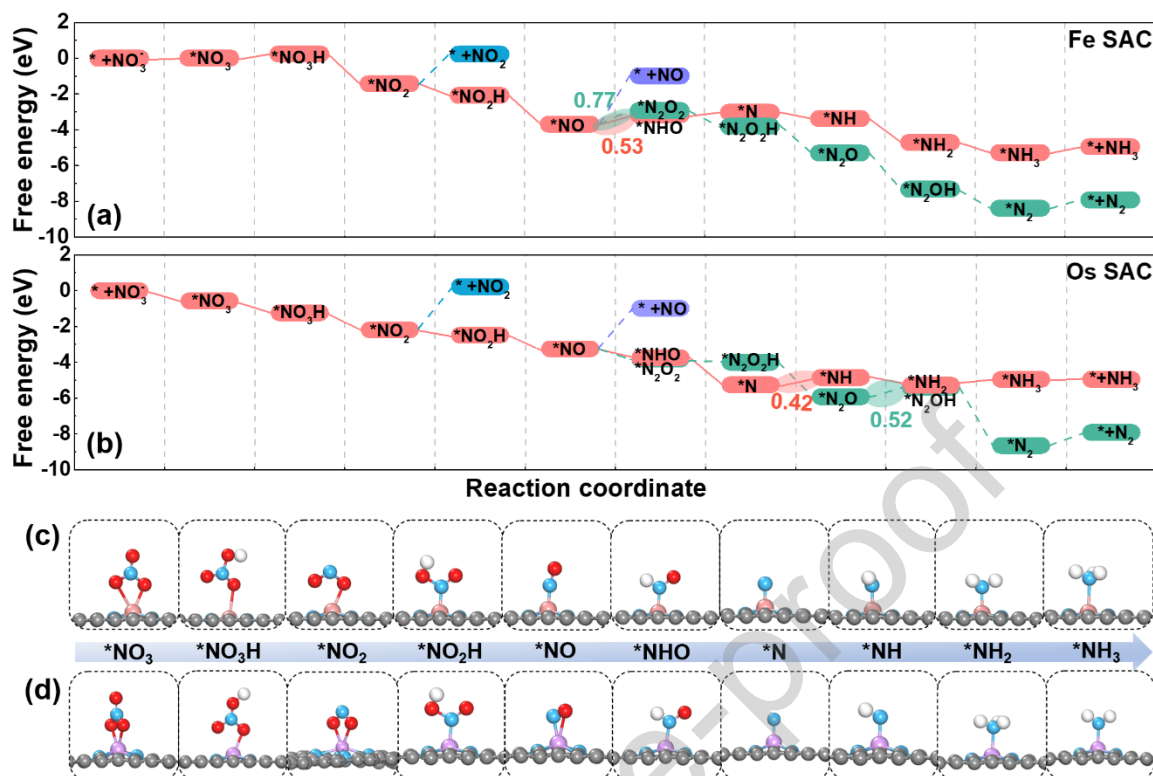


**Figure 3.** a) Summary of limiting potentials on TM SAC after screening for NO<sub>3</sub>RR via the most favorable pathway. b) NO<sub>3</sub>RR volcano plot of TM SAC with a descriptor of  $\Delta G_{\text{NO}_3}^*$ , where Os SAC and Fe SAC are almost located at the top of the volcano. c) Summarized Gibbs free energy of NH<sub>3</sub> desorption ( $\Delta G_{\text{NH}_3\text{-des}}^*$ ) on various TM SAC catalysts.

### NO<sub>3</sub>RR Performance of Fe SAC and Os SAC

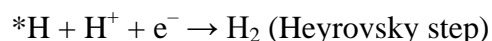
The step-by-step free energy diagrams of NO<sub>3</sub>RR on Fe SAC and Os SAC presented in **Figures 4a** and **4b** are further investigated to confirm their nitrate-to-ammonia performance. **Figures 4c** and **4d** illustrate the optimal structures of each intermediate product for NH<sub>3</sub> synthesis adsorbed on Fe SAC and Os SAC substrates (the intermediates producing N<sub>2</sub> are shown in **Figure S6**), and the distance between the adsorbed intermediate atom and the metal atom is listed in **Table S2**. For the Fe SAC in **Figure 4a**, NO<sub>3</sub><sup>-</sup> is firstly adsorbed on Fe SAC with the free energy slightly increased by 0.01 eV. Subsequently, \*NO<sub>3</sub><sup>-</sup> is hydrogenated by (H<sup>+</sup> + e<sup>-</sup>) pair to form \*NO<sub>3</sub>H intermediate, which is a slightly uphill step

with the free energy increased by 0.23 eV. Then, the free energy change suddenly dropped by  $-1.67$  eV to form  $*\text{NO}_2$ . The hydrogenation process is then proceeded to generate  $*\text{NO}_2\text{H}$  through an exothermal process. Following this,  $*\text{NO}_2\text{H}$  is attacked by a  $(\text{H}^+ + \text{e}^-)$  pair, releasing  $\text{H}_2\text{O}$ , whereas  $*\text{NO}$  stays adsorbed with the Fe-N bond. The change in the free energy profile is  $-1.62$  eV. Next, the free energy of the endothermic process from  $*\text{NO}$  to  $*\text{NHO}$  increases by 0.53 eV. In the following steps ( $*\text{NHO} \rightarrow *\text{N}$ ), H proton consecutively attacks  $*\text{NHO}$ , and the corresponding energy increases by 0.13 eV. In the subsequent steps ( $*\text{N}-*\text{NH}-*\text{NH}_2-*\text{NH}_3$ ), H proton consecutively attacks intermediates, and the corresponding energies drop by  $-0.35$ ,  $-1.33$ , and  $-0.58$  eV. The energy of 0.34 eV is eventually required during the desorption of  $\text{NH}_3$ . For Os SAC in **Figure 4b**,  $\text{NO}_3^-$  is spontaneously adsorbed on the active site with a negative  $\Delta G_{\text{NH}_3}^*$  of  $-0.57$  eV. Then, it goes through the entire exothermal process until  $*\text{N}$  is formed with energy changes of  $-0.68$ ,  $-0.95$ ,  $-0.30$ ,  $-0.76$ ,  $-0.49$ , and  $-1.53$  eV in each step. In the following three hydrogenation steps ( $*\text{N} \rightarrow *\text{NH} \rightarrow *\text{NH}_2 \rightarrow *\text{NH}_3$ ), only  $*\text{N} \rightarrow *\text{NH}$  and  $*\text{NH}_2 \rightarrow *\text{NH}_3$  are upward, and their Gibbs free energy changes are 0.42 and 0.33 eV, respectively. The final process is the release of the adsorbed  $\text{NH}_3$  with only 0.01 eV free energy changes. The formation of by-products of both Fe SAC and Os SAC, such as  $\text{NO}_2$ ,  $\text{NO}$ , and  $\text{N}_2$ , during the entire reaction process is relatively difficult, as shown in **Figure S7** (the corresponding energies increase by 2.42, 2.27, and 0.52 eV for Os SAC and 1.66, 2.71, and 0.77 eV for Fe SAC); so it can be reasonably inferred that the final synthesis of  $\text{NH}_3$  can be achieved, which is consistent with recent experimental results.<sup>48</sup> Therefore, the potential determination step (PDS) of Os SAC for the  $\text{NO}_3\text{RR}$  to ammonia is  $*\text{N} \rightarrow *\text{NH}$  with the value of 0.42 eV, whereas the PDS of Fe SAC is  $*\text{NO} \rightarrow *\text{NHO}$  with the value of 0.53 eV. The competitiveness of the hydrogen precipitation reaction (HER) must be also considered to verify the selectivity of Fe SAC and Os SAC.

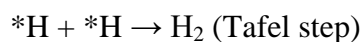


**Figure 4.** a, b) NO<sub>3</sub>RR free energy diagrams of the ideal Fe SAC and Os SAC pathways, respectively. For comparison, the paths for releasing NO<sub>2</sub>, NO, N<sub>2</sub>O, and N<sub>2</sub> are also displayed. c, d) Structures of NO<sub>3</sub>RR intermediates adsorbed on Fe SAC and Os SAC, respectively.

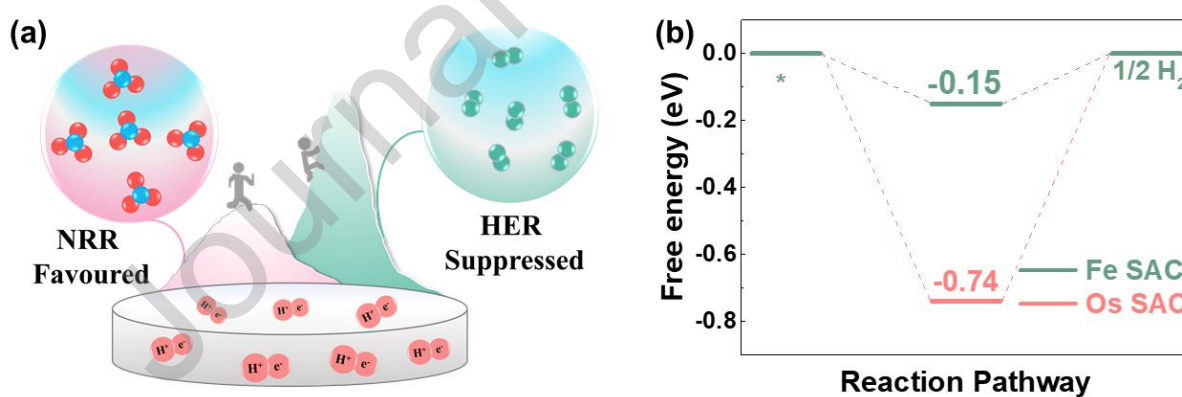
The schematic in **Figure 5a** illustrates that catalysts with excellent selectivity must satisfy the condition that the adsorption energy of NO<sub>3</sub><sup>-</sup> ( $G_{*NO_3}$ ) is more negative than that of hydrogen ( $G_{*H}$ ) to suppress HER, thereby favoring the whole reaction of NO<sub>3</sub>RR.<sup>54</sup> Generally, in the acidic solution, the overall HER pathway is:



or



where \* refers to a potential active site. The free energy diagram for the overall HER process is normally a three-state one, comprising of an initial-state ( $H^+ + e^-$ ), an intermediate-state of H adsorbed on the catalyst surface (\*H), and a final-state product represented by  $\frac{1}{2}H_2$ .<sup>55</sup> Typically, \*H is the key factor to enable favorable HER process and we use  $G_{*H}$  to determine the HER performance. **Figure 5b** shows that the  $G_{*H}$  can be referred to as Eqs. S7 and S8. The  $G_{*NO_3}$  of Fe SAC is  $-0.13$  eV, which is higher than  $G_{*H}$  ( $-0.15$  eV). This finding indicates that Fe SAC prefers to produce  $H_2$ . However, the  $G_{*NO_3}$  of Os SAC is  $-0.83$  eV, which is more negative than  $G_{*H}$  ( $-0.74$  eV). This observation further confirms that Os SAC performs poorly in HER. In summary, the above results indicate that Os SAC has high selectivity for  $NO_3RR$  to ammonia.



**Figure 5.** a) Schematic of TM SAC with better selectivity for  $NO_3RR$  than HER. b) Gibbs free energy changes for hydrogen reduction reaction on Fe SAC and Os SAC.

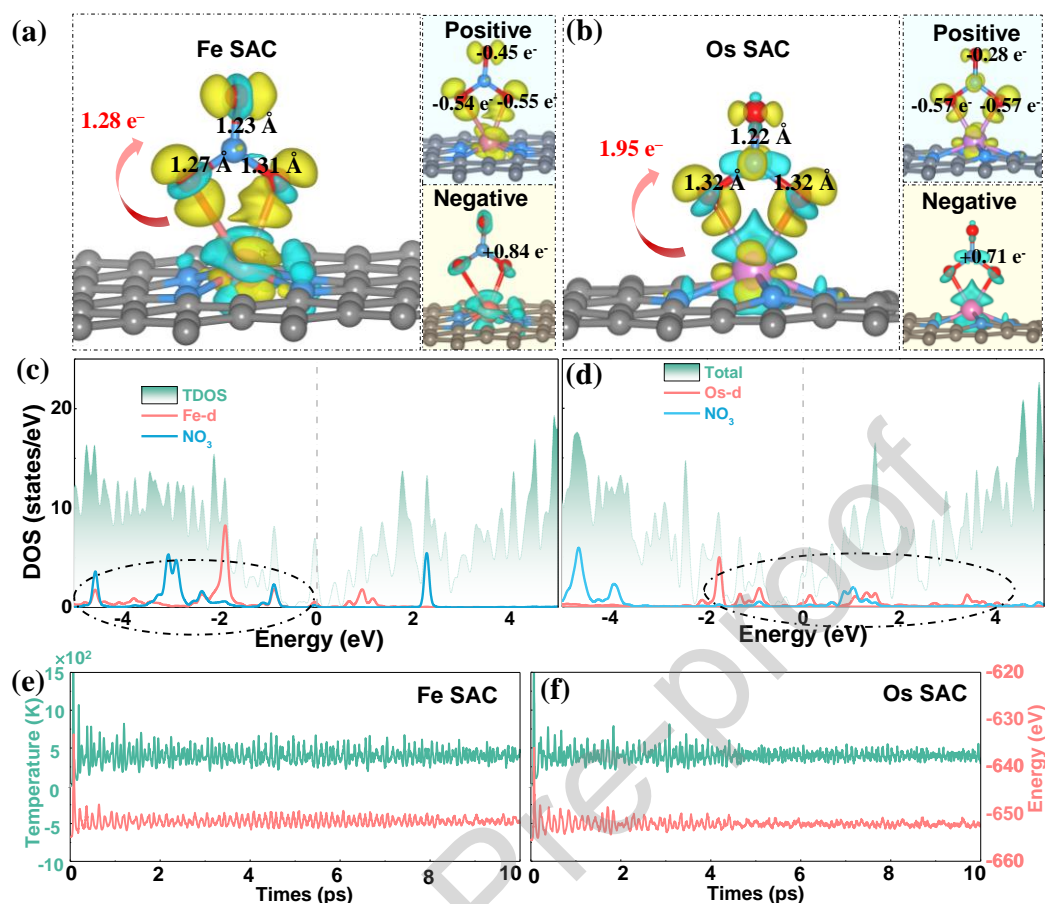
### $NO_3RR$ Activity Origin on Fe SAC and Os SAC

The first  $NO_3^-$  adsorption is the most crucial step in determining  $NO_3RR$ . As mentioned above, neither too strong nor too weak  $NO_3^-$  adsorption is conducive to the



subsequent reaction. In order to shed light on the origin of NO<sub>3</sub>RR activity, we revealed the adsorption of NO<sub>3</sub><sup>-</sup> on Os SAC from two aspects, where Fe SAC is chosen as the comparison. First, we calculated the charge density difference to indicate the charge transfer effect between NO<sub>3</sub><sup>-</sup> and the substrate. An obvious charge transfer between TM SAC and the adsorbed NO<sub>3</sub><sup>-</sup> can be observed in **Figures 6a** and **6b**. The charge transfer from TM atom to NO<sub>3</sub><sup>-</sup> (1.28 and 1.43 e<sup>-</sup> for Fe SAC and Os SAC, respectively) provides substantial evidence regarding NO<sub>3</sub><sup>-</sup> adsorption (-0.13 and -0.83 eV for Fe SAC and Os SAC, respectively), that is, the strong adsorption corresponding to the increasing charge transfer from TM atom to NO<sub>3</sub><sup>-</sup>. Moreover, the N-O bond length in the adsorbed NO<sub>3</sub><sup>-</sup> ( $d_{N-O} = 1.27/1.31 \text{ \AA}$  for Fe SAC and  $d_{N-O} = 1.32/1.32 \text{ \AA}$  for Os SAC) is considerably longer than that in the HNO<sub>3</sub> (gas,  $d_{N-O}=1.21 \text{ \AA}$ ). The increased N-O bond length and electron transfer revealed that the adsorbed NO<sub>3</sub><sup>-</sup> on Fe SAC and Os SAC is sufficiently activated. In other words, the more the number of electrons transferred from the catalyst, the more obvious the change of N-O bond length, and the better the activation of \*NO<sub>3</sub>. The electrons transferred by Os SAC are more than those transferred by Fe SAC. Thus, the performance of Os SAC for NO<sub>3</sub><sup>-</sup> activation and subsequent NO<sub>3</sub>RR activity and selectivity is better than that of Fe SAC. Second, the calculated partial density of states (PDOS) of the two candidates was further evaluated, as shown in **Figures 6c** and **6d**. The PDOS were plotted for the same energy window from -5 eV to 5 eV to facilitate comparison. Our results indicate that on Fe SAC, the 2p states of adsorbed NO<sub>3</sub><sup>-</sup> species are delocalized and weakly hybridized with Fe 3d levels throughout a narrow energy range of 4.73 eV to 0 eV. By contrast, the hybridization of the Os SAC substrate and NO<sub>3</sub><sup>-</sup> is substantially strong in a wide region between -1.98 and 4.14 eV. The presence of the pronounced hybridization on Os SAC further implies that its interaction with NO<sub>3</sub><sup>-</sup> species is too strong, resulting in a low limiting potential.





**Figure 6.** a,b) Charge density differences of  $\text{NO}_3^-$  adsorbed on Fe SAC and Os SAC. Isosurfaces are  $5 \times 10^{-3} \text{ \AA/bohr}^3$ . c,d). PDOS of  $\text{NO}_3^-$  adsorbed on Fe SAC and Os SAC, respectively. e,f) Energy and temperature evolution versus the AIMD time for Fe SAC and Os SAC, respectively. The AIMD simulation lasts for 10 ps at 500 K.

### Stability of Fe SAC and Os SAC

Material stability is an essential condition for researching catalytic characteristics. Thus, the stability of Fe SAC and Os SAC is considered by calculating the ab initio molecular dynamics (AIMD), as shown in **Figures 6e** and **6f**. The completely optimized models of Fe SAC and Os SAC are shown in **Figure S8**. The structure of Fe SAC and Os SAC is still stable after the AIMD evolved by 10,000 steps at the step length of 1 fs. No bond break exists, and the acceptable surface deformation, which oscillates around the original

configuration, is only little. It also possesses extraordinarily high thermal stability at 500 K. Fe SAC has been successfully synthesized through experiments; hence, Os SAC also has good experimental feasibility in the reaction environment and tremendous promise as a catalyst from NO<sub>3</sub>RR to NH<sub>3</sub>.

## Conclusion

In summary, we studied the activity and selectivity of a series of TM-doped nitrogen-coordinated SACs for electrocatalytic reduction of nitrate to ammonia through high-throughput first-principle calculations. We calculated different reaction paths and compared them with the energy barriers of the by-products by considering the four-step screening method and the various adsorption methods of NO. The results indicated that Fe SAC and Os SAC are located near the top of the volcano plot and have excellent limiting potentials of -0.42 and -0.53 V, respectively. In addition, the energy barriers for the formation of by-products, such as NO<sub>2</sub>, NO, N<sub>2</sub>O, and N<sub>2</sub>, are comparatively large. This finding also demonstrated that Fe SAC and Os SAC have good selectivity for NH<sub>3</sub> formation. Further calculation also illustrated that the selectivity of Os SAC against the side reaction of HER is better than that of Fe SAC. Os SAC also maintains structural stability at 500 K. Therefore, our theoretical analyses confirmed that Os SAC is a potential NO<sub>3</sub>RR electrocatalyst with excellent activity, selectivity, and stability, thereby opening new avenues for efficient nitrate degradation and ammonia production, which can decrease the time and economic cost of trial and error in the NO<sub>3</sub>RR experimental study. In the future, we will also design and develop more efficient NO<sub>3</sub>RR electrocatalysts, such as metallophthalocyanine- and metalloporphyrin-based COFs materials, which will be the focus of our research due to their well-defined crystalline porous structures together with tailored functionalities.

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### **CRedit authorship contribution statement**

**Shuo Wang** carried out the theoretical calculations and wrote the manuscript. **Shuo Wang** and **Haixing Gao** contribute equally. **Lei Li, Kwan San Hui, Zongping Shao, Kwun Nam Hui** conceived the idea writing-review & editing. **Duc Anh Dinh, Shuxing Wu, Sachin Kumar** and **Fuming Chen** contributed to the methodology and project design. All authors were involved in the analysis and discussion of the results.

### **Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

Graphical abstract

## Abstract



## Highlights

- A comprehensive screening of TM SAC candidates for stability,  $\text{NO}_3^-$  adsorption strength, catalytic activity and selectivity via high-throughput DFT calculations.
- Os SAC exhibited an outstanding performance with a low overpotential of only 0.42 V.
- The increasing charge transfer from TM atom to  $\text{NO}_3^-$  lead to the strong hybridization of the Os SAC substrate and  $\text{NO}_3^-$ , then improve the catalytic performance.